| Subject Code | Q Id | Questions | Answ Key |
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| 603 | 3601 | Isotopes are atoms of <br> (A) the same element with different masses <br> (B) the same element with same masses <br> (C) different element with same mass <br> (D) different elements with different masses | (A) |
| 603 | 3602 | different elements with different masses <br> (A) 44 grams <br> (B) 88 grams <br> (C) 176 grams <br> (D) 132 grams | (C) |
| 603 | 3603 | In a test, 20 kg of propane was burnt with 400 kg of air to produce 44 kg of CO 2 and 12 kg CO . What was the percent excess air? <br> (A) 2.27 <br> (B) 28 <br> (C) 13.79 <br> (D) 2.8 | (B) |
| 603 | 3604 | One gram of a sample of crude sulfur is completely burnt in air. The weight of sulfur dioxide formed is 1.5 grams. The purity of sulfur sample is <br> (A) $100 \%$ <br> (B) $75 \%$ <br> (C) $50 \%$ <br> (D) $65 \%$ | (B) |
| 603 | 3605 | What is percentage carbon in ammonium carbonate, (NH4)2 CO3? <br> (A) 12.50 <br> (B) 6.25 <br> (C) 25.0 <br> (D) 12.0 | (A) |
| 603 | 3606 | A cooking gas cylinder can withstand a pressure of 15 atm . The pressure gauge of the cylinder indicates 12 atm at 27 C C.During a sudden fire in the building the temperature starts rising. At what temperature will the cylinder explode? <br> (A) 33.75 C <br> (B) $102 \geqslant \mathrm{C}$ <br> (C) $40 \geqslant \mathrm{C}$ <br> (D) 240 K | (B) |
| 603 | 3607 | Weight of 56 litres of ammonia at S.T.P. is $\qquad$ gram. <br> (A) 2.5 <br> (B) 8600 <br> (C) 42.5 <br> (D) 4.56 | (C) |
| 603 | 3608 |  | (C) |


|  |  | A gas at $0<\mathrm{C}$ is cooled at constant pressure until its volume becomes half the original volume. The temperature of the gas at this state will be <br> (A) $-273 仓 \mathrm{C}$ <br> (B) $-136.5 \geqslant \mathrm{~K}$ <br> (C) $-136.5 \geqslant \mathrm{C}$ <br> (D) $0 \geqslant \mathrm{~K}$ |  |
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| 603 | 3609 | „COX chart" is a plot of <br> (A) Vapor pressure vs temperature <br> (B) $\log$ (vapor pressure) vas $\log$ (temperature) <br> (C) $\log$ (vapor pressure) vs temperature <br> (D) Log (vapor pressure) vs inverse of temperature | (D) |
| 603 | 3610 | The vapor pressures of benzene and toluene are 3 and $4 / 3$ atmospheres respectively. The vapor phase mole fraction of benzene in equilibrium with a liquid mixture of 0.4 moles of benzene and 0.6 moles of toluene is: <br> (A) 0.8 <br> (B) 0.6 <br> (C) 0.2 <br> (D) 0.4 | (B) |
| 603 | 3611 | The critical point of a substance represents <br> (A) a point (pressure and temperature) where all three phases of the substance coexist in equilibrium. <br> (B) The lowest pressure and temperature where vapor and liquid phases coexist in equilibrium <br> (C) A temperature where vapor is transformed into liquid <br> (D) The highest pressure and temperature where all thermodynamic properties of the liquid and vapor are identical | (D) |
| 603 | 3612 | A gas can always be condensed by <br> (A) cooling alone <br> (B) compressing alone <br> (C) cooling below the critical temperature and then compressing <br> (D) bringing it below triple point | (C) |
| 603 | 3613 | Alkyl benzene sulfonate (ABS) is a <br> (A) detergent <br> (B) synthetic rubber <br> (C) plasticizer <br> (D) an industrial solvent | (A) |
| 603 | 3614 | Poly Tetra Fluro Ethylene (PTFE) is popularly known as <br> (A) Perspex <br> (B) Bakelite <br> (C) pidilite <br> (D) Teflon | (D) |
| 603 | 3615 | When small particles are settling in a fluid, at very low Reynolds numbers, the flow is described by <br> (A) streamline flow <br> (B) rotational flow <br> (C) creeping flow | (C) |


|  |  | (D) irrotational flow |  |
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| 603 | 3616 | A solid particle is moving through a fluid and the particle Reynolds number is 0.24 ; the drag coefficient is <br> (A) 1 <br> (B) 10 <br> (C) 100 <br> (D) 1000 | (A) |
| 603 | 3617 | In fluid flow at low Reynolds numbers <br> (A) viscous forces are important <br> (B) Inertial forces are important <br> (C) Buoyancy forces are important <br> (D) Gravitational forces are important | (A) |
| 603 | 3618 | Two circular pipes have different diameters but same roughness. Water is flowing through pipe 1 , having friction factor fl at a Reynolds number of 12,000 ; air is flowing through pipe 2, having friction factor $\mathfrak{f} 2$ at the same Reynolds of 12,000 . Then <br> (A) f1 $>$ f 2 <br> (B) $\mathrm{f} 2<\mathrm{f} 1$ <br> (C) $\mathrm{f} 1=\mathrm{f} 2$ <br> (D) f1 and f2 cannot be calculated | (C) |
| 603 | 3619 | For standard steel pipes, for a given NPS, as schedule number increases, wall thickness <br> (A) increases <br> (B) decreases <br> (C) remains same <br> (D) schedule number has nothing to do with wall thickness | (A) |
| 603 | 3620 | The discharge is proportional to square root of the head for <br> (A) orifice meter <br> (B) V-notch <br> (C) sutro-weir <br> (D) rectangular notch | (A) |
| 603 | 3621 | The Fanning friction factor for turbulent flow is a where NRe is Reynolds number and $\mathrm{E} / \mathrm{D}$ is relative roughness. <br> (A) function of NRe only <br> (B) function of $\mathrm{E} / \mathrm{D}$ and Nre <br> (C) function of $\mathrm{E} / \mathrm{D}$ only <br> (D) constant | (B) |
| 603 | 3622 | The hydraulic diameter of a duct having the shape of an equilateral triangle with side a is <br> (A) $\sqrt{3} \cdot a$ <br> (B) $\sqrt{3} \cdot \mathrm{a} / 4$ <br> (C) | (C) |


|  |  | $a / \sqrt{3}$ <br> (D) $a / 4 \sqrt{3}$ |  |
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| 603 | 3623 | When a material is subjected to an increased shear rate, an increase in its apparent viscosity occurs; such a phenomenon is observed in <br> (A) dilatants <br> (B) rheopectics <br> (C) viscoelastics <br> (D) thixotropics. | (A) |
| 603 | 3624 | Water is flowing under laminar conditions in a pipe of length L. If the diameter of the pipe is doubled, for a constant volumetric flow rate, the pressure drop across the pipe <br> (A) decreases 2 times <br> (B) decreases 16 times <br> (C) increases 2 times <br> (D) increases 16 times | (B) |
| 603 | 3625 | The plot below corresponds to <br> (A) Pseudo plastic fluid <br> (B) real fluid <br> (C) Bingham plastic <br> (D) None of the above | (C) |
| 603 | 3626 | Diaphragm pumps are used to handle <br> (A) highly viscous liquids <br> (B) liquids to be pumped into high pressure vessels <br> (C) hazardous or toxic liquids / slurries <br> (D) liquids having very low vapor pressure | (A) |
| 603 | 3627 | The net positive suction head (NPSH) of a centrifugal pump is defined as the sum of the velocity head and the pressure head at th <br> (A) suction <br> (B) discharge minus vapor pressure of the liquid at the discharge temperature <br> (C) discharge <br> (D) suction minus vapor pressure of the liquid at suction temperature | (D) |


| 603 | 3628 | Froude number is a ratio of <br> (A) inertial forces to gravity force <br> (B) buoyant forces to gravity force <br> (C) inertial forces to viscous forces <br> (D) inertial forces to buoyant forces | (A) |
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| 603 | 3629 | Cavitation in a centrifugal pump may be avoided by maintaining <br> (A) a very low suction head <br> (B) a positive suction head <br> (C) a very low discharge head <br> (D) the suction and discharge valves properly | (B) |
| 603 | 3630 | Bernoulli"es theorem deals with the law of conservation of <br> (A) energy <br> (B) mass <br> (C) momentum <br> (D) gravity | (A) |
| 603 | 3631 | The loss of pressure head for the laminar flow through pipes varies as the <br> (A) square of velocity <br> (B) proportional to the velocity <br> (C) inverse of the velocity <br> (D) inverse of the square of the velocity | (B) |
| 603 | 3632 | For hydraulically smooth pipe, the resistance to flow depends only on the <br> (A) flow Reynolds number <br> (B) relative roughness <br> (C) absolute roughness <br> (D) Reynolds number and relative roughness | (A) |
| 603 | 3633 | The discharge co-efficient for a venturimeter is found to be a function of <br> (A) meter size <br> (B) Reynolds number <br> (C) Both (A) and (B) <br> (D) None of the above | (C) |
| 603 | 3634 | Newton"s Law of viscosity states that the shear stress is directly proportional to the <br> (A) velocity <br> (B) velocity gradient <br> (C) square of velocity <br> (D) square of velocity gradient | (B) |
| 603 | 3635 | Vena contracta is found in <br> (A) Rotameter <br> (B) orificemeter <br> (C) bourdon tube pressure gauge <br> (D) wet gas flow meter | (B) |


| 603 | 3636 | The unit of kinematic viscosity is <br> (A) $\mathrm{m}^{2} / \mathrm{s}$ <br> (B) Stoke <br> (C) either (a) or (b) <br> (D) poise | (C) |
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| 603 | 3637 | Flow of incompressible fluid with no shear is called <br> (A) creep flow <br> (B) stream line flow <br> (C) potential flow <br> (D) boundary layer flow | (C) |
| 603 | 3638 | For precise control of fluid flow rate the best performance is obtained by <br> (A) gate valve <br> (B) check valve <br> (C) globe valve <br> (D) None of the above | (C) |
| 603 | 3639 | Compared to gate valve pressure drop is $\qquad$ in globe valve. <br> (A) less <br> (B) more <br> (C) same <br> (D) unpredictable | (B) |
| 603 | 3640 | Turbulent velocity profile becomes flatter and flatter with $\qquad$ <br> (A) decreasing Reynolds number <br> (B) increasing Reynolds number <br> (C) at a given Reynolds number <br> (D) None of the above | (B) |
| 603 | 3641 | In turbulent flow, mean velocity in a circular pipe is approximately equal to <br> (A) 0.8 to 0.82 of maximum velocity <br> (B) 0.9 to 0.95 of maximum velocity <br> (C) 0.5 of maximum velocity <br> (D) 0.6 to 0.65 of maximum velocity | (A) |
| 603 | 3642 | For closer sizing of solid particles, intermediate screens are available in Tyler standard screen series; the ratio of the actual mesh dimension of any screen in intermediate range to that of the next smaller screen is <br> (A) 1.414 <br> (B) 0.707 <br> (C) 1.189 <br> (D) 0.841 | (A) |
| 603 | 3643 | Kynch theory is used in the design of <br> (A) classifiers <br> (B) centrifugal separators <br> (C) filters <br> (D) clarifiers | (D) |


| 603 | 3644 | For settling in the stokes range the value of Reynolds number is <br> (A) 2 <br> (B) 200 <br> (C) 500 <br> (D) 0 | (D) |
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| 603 | 3645 | LMTD correction factor is used in the design of <br> (A) double pipe heat exchangers <br> (B) shell and tube condensers <br> (C) single pass shell and tube heat exchangers <br> (D) multipass shell and tube heat exchangers | (D) |
| 603 | 3646 | Which has the lowest Prandtl number? <br> (A) organic liquids <br> (B) inorganic liquids <br> (C) liquid metals <br> (D) gases | (C) |
| 603 | 3647 | Heat exchangers which are especially useful with food products and similar heat- sensitive materials are <br> (A) extended-surface exchangers <br> (B) plate exchangers <br> (C) scraped-surface exchangers <br> (D) double-pipe exchangers | (C) |
| 603 | 3648 | The mode of heat transfer in microwave ovens used for baking food is <br> (A) conduction <br> (B) convection <br> (C) radiation <br> (D) combined convection and conduction | (C) |
| 603 | 3649 | The maximum heat loss from a heated pipe occurs when the thickness of thermal insulation is $\qquad$ <br> (A) less than critical radius <br> (B) equal to critical radius <br> (C) more than critical radius <br> (D) both (b) and | (B) |
| 603 | 3650 | In a cooling tower water is cooled from $95 \geqslant \mathrm{C}$ to $80 \geqslant \mathrm{C}$ by exposure to air with a wet bulb temperature of $70 \geqslant \mathrm{C}$. The approach would be <br> (A) $15 \geqslant \mathrm{C}$ <br> (B) $10 \geqslant \mathrm{C}$ <br> (C) $25 \geqslant \mathrm{C}$ <br> (D) None of the above | (B) |
| 603 | 3651 | In a heat exchanger with steam outside the tubes, a liquid gets heated to $45 \geqslant \mathrm{C}$, when its flow velocity in the tubes is $2 \mathrm{~m} / \mathrm{s}$. If the flow velocity is reduced to $1 \mathrm{~m} / \mathrm{s}$, other things remaining the same, the temperature of the exit liquid will be <br> (A) equal to $45 \geqslant \mathrm{C}$ <br> (B) initially decreases and remains constant thereafter <br> (C) less than $45 \geqslant \mathrm{C}$ <br> (D) more than $45 \geqslant \mathrm{C}$ | (D) |


| 603 | 3652 | Name the process in which heat transfer is undesirable and its flow is to be prevented <br> (A) gas turbine blades <br> (B) Wall of steam pipes <br> (C) wall of internal combustion chamber <br> (D) outer space vehicles | (B) |
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| 603 | 3653 | Name the method by which heat transfer takes place due to direct molecular communication without any appreciable displacement of the system <br> (A) forced convection <br> (B) Natural convection <br> (C) conduction <br> (D) radiation | (C) |
| 603 | 3654 | The thermal conductivity of perfect heat insulator is <br> (A) Zero <br> (B) One <br> (C) between 0 and infinity <br> (D) infinity | (A) |
| 603 | 3655 | If the pipe radius ( $r$ ) is less than critical radius $\left(r_{c}\right)$, the heat loss from pipe <br> (A) decreases with the addition of insulation until $r=r_{c}$ <br> (B) increases with the addition of insulation until $r=r_{c}$ <br> (C) increases with the addition of insulation <br> (D) decreases with the addition of insulation | (B) |
| 603 | 3656 | All substances emit energy in the form of radiation continuously at a temperature of <br> (A) above absolute zero temperature <br> (B) above 0 oC <br> (C) above 100 oC <br> (D) above its decomposition temperature | (A) |
| 603 | 3657 | 2-4 shell and tube heat exchanger means <br> (A) 2 shell side pass and 4 tube side pass <br> (B) 4 shell side pass and 2 tube side pass <br> (C) 2 shell side pass and 2 tube side pass <br> (D) 4 shell side pass and 4 tube side pass | (A) |
| 603 | 3658 | Mass dispersion may be characterized by the dimensionless group <br> (A) Sherwood number <br> (B) Peclet number <br> (C) Fourier number <br> (D) Froude number | (A) |
| 603 | 3659 | In general the diffusivity DAB in a liquid varies with temperature as <br> (A) $\mathrm{T}^{1.5}$ <br> (B) T <br> (C) $1 / \mathrm{T}$ | (B) |


|  |  | (D) $\mathrm{T}^{1.75}$ |  |
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| 603 | 3660 | J flux is the molar flux with reference to <br> (A) Moving frame of reference <br> (B) Fixed frame of reference <br> (C) None of the above <br> (D) May be a) or b) | (A) |
| 603 | 3661 | The gas phase reaction $2 A+B \leftrightarrow C+D$ occurs on the surface of a catalyst pellet at steady state. If the reaction is mass transfer controlled, then what is the flux ratio $\mathrm{N}_{\mathrm{A}} / \mathrm{N}_{\mathrm{C}}$ ? <br> (A) -2 <br> (B) -0.5 <br> (C) 2 <br> (D) 0.5 | (A) |
| 603 | 3662 | Knudsen diffusion occurs when the ratio of pore diameter to mean free path of molecules is <br> (A) less than 0.20 <br> (B) greater than 0.20 <br> (C) less than 2.0 <br> (D) greater than 2.0 | (A) |
| 603 | 3663 | For structure dependent diffusion in a solid the ratio of Effective diffusivity to Binary diffusivity <br> (A) varies and depends on temperature <br> (B) varies and depends on pressure <br> (C) varies and depends on component diffusing <br> (D) remains constant and depends on pore geometry | (D) |
| 603 | 3664 | For the boundary layer development on a flat plate during convective mass transport, the velocity profile will be identical to concentration profile, when Schmidt number is equal to <br> (A) 0 <br> (B) 1 <br> (C) between 0 and 1 <br> (D) more than 1 | (B) |
| 603 | 3665 | Distillation can be used for the separation of components from a liquid mixture only if the operating temperature is <br> (A) above the dew point temperature <br> (B) below the bubble point temperature <br> (C) between the bubble point and dew point temperature <br> (D) All of the above | (C) |
| 603 | 3666 | In a binary mixture, separation is very efficient when the relative volatility is <br> (A) 0 <br> (B) 1 <br> (C) between 0 and 1 <br> (D) more than 1 | (D) |
| 603 | 3667 | An azeotropic solution of two liquids has boiling point lower than either of them, when it | (C) |


|  |  | (A) is unsaturated <br> (B) is saturated <br> (C) shows negative deviation from Raoult's law. <br> (D) shows positive deviation from Raoult's law |  |
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| 603 | 3668 | If the feed to distillation column is a subcooled liquid, then $q$ line is <br> (A) Vertical <br> (B) horizontal <br> (C) line with a positive slope <br> (D) line with a negative slope | (C) |
| 603 | 3669 | In a binary mixture, separation is very efficient when the relative volatility is <br> (A) 0 <br> (B) 1 <br> (C) more than 1 <br> (D) between 0 and 1 | (C) |
| 603 | 3670 | The feed to a distillation column is changed from saturated liquid to saturated vapour. If the separation and reflux ratio remains unchanged ,the number of ideal stages will <br> (A) increase <br> (B) decrease <br> (C) remain constant <br> (D) cannot say | (A) |
| 603 | 3671 | The washing of ammonia from a mixture of ammonia and air by means of liquid water is an example of <br> (A) gas absorption <br> (B) gas adsorption <br> (C) gas desorption <br> (D) gas stripping | (A) |
| 603 | 3672 | In case of a gas absorber <br> (A) equilibrium curve lies below the operating line <br> (B) equilibrium curve lies above the operating line <br> (C) equilibrium curve lies above or below the operating line <br> (D) None of the above | (A) |
| 603 | 3673 | In an azeotropic mixture the equilibrium liquid composition is <br> (A) more than vapour composition <br> (B) same as vapour composition <br> (C) less than vapour composition <br> (D) independent of pressure | (B) |
| 603 | 3674 | Down comer flooding occurs in plate columns at <br> (A) low gas and liquid rates <br> (B) high gas and low liquid rates <br> (C) high gas and liquid rates <br> (D) low gas and high liquid rates | (C) |
| 603 | 3675 | In the design and operation of packed towers the operating velocity is ---- percentage of flooding velocity | (A) |


|  |  | (A) 70 and 85 <br> (B) 85 and 95 <br> (C) 50 and 60 <br> (D) 60 and 65 |  |
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| 603 | 3676 | In the design of towers used for mass transfer operations, the tower diameter is computed based on the considerations of <br> (A) mass transfer <br> (B) pressure drop <br> (C) flooding <br> (D) ratio of flow rates of phases | (C) |
| 603 | 3677 | Improved gas absorption can be achieved by carrying out the process at <br> (A) low temperature and high pressure <br> (B) high temperature and low pressure <br> (C) high temperature and high pressure <br> (D) low temperature and low pressure | (A) |
| 603 | 3678 | A column is designed to operate at a reflux ratio of 1.3 (saturated reflux).In actual operation the reflux is well below its bubble point. What reflux ratio would you suggest qualitatively? <br> (A) $\mathrm{R}>1.3$ <br> (B) $\mathrm{R}<1.3$ <br> (C) 1.3 <br> (D) $\mathrm{R}=0$ | (B) |
| 603 | 3679 | When a packed tower is operated close to flooding condition, we will have <br> (A) more pressure drop and higher mass transfer <br> (B) more pressure drop and lower mass transfer <br> (C) lower pressure drop and higher mass transfer <br> (D) lower pressure drop and lower mass transfer | (B) |
| 603 | 3680 | For distillation of heat sensitive materials <br> (A) Atmospheric pressure is preferred <br> (B) pressures above atmospheric pressure are preferred <br> (C) vacuum conditions are preferred <br> (D) pressure has no effect | (C) |
| 603 | 3681 | In a gas -liquid mass transfer operation if the gas side film mass transfer coefficient is much higher than the liquid side mass transfer coefficient, then the rate of mass transfer <br> (A) is gas film controlled <br> (B) is liquid film controlled <br> (C) can be enhanced by increasing the turbulence in the gas phase <br> (D) can be enhanced by decreasing the gas film thickness | (B) |
| 603 | 3682 | Freundlich isotherm relates <br> (A) mass of solute adsorbed per unit mass of adsorbent with the concentration of solute in the liquid phase at equilibrium <br> (B) Equilibrium compositions in gas and liquid phase <br> (C) Liquid-liquid equilibrium relationship <br> (D) None of the above | (A) |


| 603 | 3683 | For multistage cross-current adsorption operation, the stage operating lines lie <br> (A) above the equilibrium curve with positive slopes <br> (B) above the equilibrium curve with negative slopes <br> (C) below the equilibrium curve with negative slopes <br> (D) below the equilibrium curve with positive slopes | (C) |
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| 603 | 3684 | Flash distillation is suitable for separation of components <br> (A) which form an azeotrope <br> (B) having very close boiling points <br> (C) having very wide boiling points <br> (D) one of which having a very high boiling point and other an impurity | (C) |
| 603 | 3685 | When a liquid is converted to vapour, entropy <br> (A) Becomes zero <br> (B) decreases <br> (C) increases <br> (D) remains the same | (C) |
| 603 | 3686 | The activity of ith species in a homogeneous solution (ai) can be defined as <br> (A) $a_{i}=f_{i} f_{i}^{0}$ <br> (B) $a_{i}=f_{i} / f_{i}^{0}$ <br> (C) $a_{i}=f_{i}^{0} / f_{i}$ <br> (D) $a_{i}=\sqrt{f_{i} f_{i}^{0}}$ | (B) |
| 603 | 3687 | A polytropic process $\mathrm{PV}^{\mathrm{n}}=$ constant for which n is infinity is a <br> (A) constant pressure process <br> (B) constant volume process <br> (C) constant temperature process <br> (D) reversible adiabatic process | (B) |
| 603 | 3688 | Find the change in internal energy when 50 g of air is heated from $25 \geqslant \mathrm{C}$ to $27 \geqslant \mathrm{C}$. The specific heat at constant volume is $0.184 \mathrm{cal} / \mathrm{g} / \geqslant \mathrm{C}$ <br> (A) 0.184 cal <br> (B) 184 cal <br> (C) 18.4 cal <br> (D) None of these | (C) |
| 603 | 3689 | An adiabatic system can exchange energy with its surroundings <br> (A) only in the form of work <br> (B) either in the form of heat or work <br> (C) in the form only heat | (A) |


|  |  | (D) both in the form of heat and work |  |
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| 603 | 3690 | For a reversible adiabatic change, the change in entropy of the system is <br> (A) Zero <br> (B) positive <br> (C) negative <br> (D) None of the above | (A) |
| 603 | 3691 | At $60<$ C, vapour pressure of methanol and water are 84.562 kPa and 19.953 kPa respectively. An aqueous solution of methanol at $60<$ C exerts a pressure of 39.223 kPa ; the liquid phase and vapour phase mole fractions of methanol are 0.1686 and 0.5714 respectively. Activity co-efficient of methanol is <br> (A) 1.572 <br> (B) 1.9398 <br> (C) 3.389 <br> (D) 4.238 | (A) |
| 603 | 3692 | In case of $\qquad$ process, the temperature of the system increases. <br> (A) Adiabatic compression <br> (B) isothermal compression <br> (C) isothermal expansion <br> (D) adiabatic expansion | (A) |
| 603 | 3693 | You turn off water flowing into the tube and open the drain. This is an example of <br> (A) an open steady-state system <br> (B) an open unsteady-state system <br> (C) closed system <br> (D) None of the above | (B) |
| 603 | 3694 | Which of the following is an extensive property? <br> (A) Temperature <br> (B) Pressure <br> (C) Volume <br> (D) Density | (C) |
| 603 | 3695 | Reactions which are very temperature - sensitive are the <br> (A) reactions with high activation energies <br> (B) reactions with low activation energies <br> (C) reversible reactions <br> (D) irreversible reactions | (B) |
| 603 | 3696 | Addition of inert gas in a reversible chemical reaction favors the forward reaction when <br> (A) $\Delta \mathrm{n}=0$ <br> (B) $\Delta \mathrm{n}>0$ <br> (C) $\Delta \mathrm{n}<0$ <br> (D) Any of the above | (B) |
| 603 | 3697 | The ratio of volume of mixed reactor to the volume of P.F.R. (for identical flow rate, feed composition and conversion) for zero order reaction is <br> (A) $\infty$ | (C) |


|  |  | $(\mathrm{B})>1$ <br> (C) 1 <br> (D) 0 |  |
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| 603 | 3698 | When a zero-order reaction is carried out in a batch reactor, the time needed for the reactant concentration to become zero is where CAO is the initial concentration of reactant A and K is the reaction velocity constant. <br> (A) <br> $\frac{1}{K}$ <br> (B) <br> CAO <br> $\overline{2 K}$ <br> (C) <br> $\frac{C_{A 0}}{K}$ <br> (D) $\frac{0.693}{K}$ | (C) |
| 603 | 3699 | When the order of a reaction is greater than unity, as the initial concentration of reactant increases the half - life of the reaction <br> (A) Remains same <br> (B) decreases <br> (C) increases <br> (D) increases and then decreases | (B) |
| 603 | 3700 | Auto catalytic reactions occur with <br> (A) the catalyst as one of the reactants <br> (B) with one of the reaction products acting as a catalyst <br> (C) temperature continuously increasing or decreasing <br> (D) biocatalysts | (B) |
| 603 | 3701 | increases 1.414 times as the reactant concentration is doubled. What could be the order of reaction? <br> (A) 0.5 <br> (B) 1.0 <br> (C) 1.5 <br> (D) 2.0 | (A) |
| 603 | 3702 | When a reversible reaction is carried out in the presence of a catalyst <br> (A) The speed of forward reaction is increased and that of backward reaction is decreased. <br> (B) The speed of forward reaction is increased to a larger extent than that of backward reaction. <br> (C) The speed of backward reaction is increased and that of forward reaction is decreased. <br> (D) The speeds of both forward and backward reactions are increased to the same extent. | (D) |
| 603 | 3703 | A zero-order reaction is carried out in an ideal PFR and MFR having equal volumes and operating under identical conditions. The ratio of conversions K1KCAO2KCAOK693.0 13 achieved in PFR to MFR will be <br> (A) $<1$ <br> (B) 1 <br> (C) $>1$ <br> (D) 2 | (B) |


| 603 | 3704 | When complete back-mixing prevails in a flow vessel, the vessel dispersion number will be <br> (A) zero <br> (B) infinity <br> (C) less than unity <br> (D) greater than unity | (B) |
| :---: | :---: | :---: | :---: |
| 603 | 3705 | It is desirable to achieve maximum decomposition in the reaction $\mathrm{N}_{2} \mathrm{O}_{4}(\mathrm{~g}) \rightarrow 2 \mathrm{NO}_{2}(\mathrm{~g}): \Delta \mathrm{H}^{\circ}{ }_{298}=57.2 \mathrm{KJ}$ So, the reaction should be carried out at <br> (A) high pressure and high temperature <br> (B) low pressure and high temperature <br> (C) high pressure and low temperature <br> (D) low pressure and low temperature | (B) |
| 603 | 3706 | A pulse of tracer is injected into the inflow of a tubular flow system in which ideal plug flow prevails; the response appears at a time equals to where $\tau$ is the space time. <br> (A) <br> 0 <br> (B) <br> $\tau$ <br> (C) <br> $0.5 \tau$ <br> (D) <br> $2 \tau$ | (B) |
| 603 | 3707 | When a reaction occurs between gas and liquid phases (reaction is very fast) and gas is sparingly soluble in liquid, it is likely that the global process is controlled by <br> (A) mass transfer through gas film <br> (B) mass transfer through liquid film <br> (C) chemical reaction <br> (D) mass transfer and chemical reaction | (B) |
| 603 | 3708 | For a porous catalyst particle "effectiveness factor" may be need as a measure to find whether the <br> (A) catalyst formulation is good for a given reaction <br> (B) reaction rate is lowered because of pore diffusional resistance <br> (C) reaction is surface reaction - controlled <br> (D) reaction is adsorption / desorption - controlled | (B) |
| 603 | 3709 | The problem of hot spots may occur in <br> (A) trickle bed reactors <br> (B) packed bed reactors <br> (C) fluidized bed reactors <br> (D) moving bed reactors | (B) |
| 603 | 3710 | The problem of "off-set" usually occurs with <br> (A) derivative control <br> (B) integral control <br> (C) proportional control | (C) |


|  |  | (D) PI control |  |
| :---: | :---: | :---: | :---: |
| 603 | 3711 | An open tank is discharging water to the open atmosphere through a valve; the discharge (volumetric flow rate) is proportional to head available in the tank. The ratio of time constant of the system to hold up time is <br> (A) 0.5 <br> (B) 1.0 <br> (C) 1.5 <br> (D) 2.0 | (B) |
| 603 | 3712 | For an under damped system, the damping coefficient is <br> (A) zero <br> (B) less than unity <br> (C) unity <br> (D) greater than unity | (B) |
| 603 | 3713 | A typical U-tube manometer filled with mercury or water would be <br> (A) an under damped system <br> (B) a over damped system <br> (C) a critically damped system <br> (D) a first-order system | (A) |
| 603 | 3714 | In the response of a first-order system to sinusoidal inputs, at higher frequencies the phase-lag approaches a limit of <br> (A) $-90^{\circ}$ <br> (B) $-45^{\circ}$ <br> (C) $-30^{\circ}$ <br> (D) $-60^{\circ}$ | (A) |
| 603 | 3715 | The resistance of a first order system is <br> (A) driving force/ flow <br> (B) storage/driving force <br> (C) flow/ driving force <br> (D) None of the above | (A) |
| 603 | 3716 | Time constant of mercury in glass thermometer (without covering or air gap) is equal to Where $m$ is mass of mercury in tube $\mathrm{C}_{\mathrm{p}}$ is the heat capacity of mercury, h is the film coefficient of heat transfer, A is the surface area of bulb for heat transfer. <br> (A) $\frac{m C_{p}}{h A}$ <br> (B) $\frac{h A}{m C_{p}}$ <br> (C) <br> $m C_{p} h A$ <br> (D) $\frac{1}{m C_{p} h A}$ | (A) |
| 603 | 3717 | If two tanks each with time constant $\tau$ are connected in interacting manner, the transfer function relating the outlet flow (Q2) to | (C) |


|  |  | the inlet flow $(\mathrm{Q})$ to this two tank system is <br> (A) $\frac{Q_{2}(s)}{Q(s)}=\frac{2}{\tau s+1}$ <br> (B) $\frac{Q_{2}(s)}{Q(s)}=\left(\frac{1}{\tau s+1}\right)^{2}$ <br> (C) $\frac{Q_{2}(s)}{Q(s)}=\frac{1}{\tau^{2} s^{2}+3 \tau s+1}$ <br> (D) $\frac{Q_{2}(s)}{Q(s)}=\left(\frac{2}{\tau s^{2}+3 \tau s+1}\right)^{2}$ |  |
| :---: | :---: | :---: | :---: |
| 603 | 3718 | The step input to a system with the transfer function $\quad \frac{Y(s)}{X(s)}=\frac{1}{s^{2}+8 s+4}$ gives a response which is <br> (A) Under damped <br> (B) oscillatory <br> (C) over damped <br> (D) critically damped | (C) |
| 603 | 3719 | A proportional controller is used to control temperature within the range of 60 to $100 \geqslant \mathrm{C}$. The controller is adjusted so that the output pressure goes from $3 \mathrm{~kg} / \mathrm{cm} 2$ (valve fully open) to $15 \mathrm{~kg} / \mathrm{cm} 2$ (valve fully closed) as measured temperature goes from 71 to $75 仓 \mathrm{C}$ with the set point held constant. Now the value of gain and proportional band is <br> (A) $3 \mathrm{~kg} / \mathrm{cm}^{2} / \mathrm{C}$ and $5 \%$ respectively <br> (B) $3 \mathrm{~kg} / \mathrm{cm}^{2} / \mathrm{C}$ and $10 \%$ respectively <br> (C) $5 \mathrm{~kg} / \mathrm{cm}^{2} / \mathrm{C}$ and $10 \%$ respectively <br> (D) $10 \mathrm{~kg} / \mathrm{cm}^{2} / \mathrm{C}$ and $3 \%$ respectively | (B) |
| 603 | 3720 | At the corner frequency, the amplitude ratio for the sinusoidal response of a first order system is <br> (A) <br> $\frac{K}{\sqrt{2}}$ <br> (B) <br> $\sqrt{2} \mathrm{~K}$ <br> (C) <br> $\sqrt{2 K}$ <br> (D) $\sqrt{\frac{K}{2}}$ | (A) |
| 603 | 3721 | In a chemical reactor, following a change in the inlet concentration of the reactant outlet concentration tends to change. The outlet concentration of the reactant is to be controlled. This control problem is called as <br> (A) Servo control <br> (B) on-off control | (C) |


|  |  | (C) regulator control <br> (D) inherent control |  |
| :---: | :---: | :---: | :---: |
| 603 | 3722 | Routh test for stability of control systems uses <br> (A) open-loop transfer function <br> (B) closed loop transfer function <br> (C) characteristic equation <br> (D) None of the above | (C) |
| 603 | 3723 | Iron sheets and pipes are usually galvanized for protection; the metal used in this process is <br> (A) nickel <br> (B) chromium <br> (C) zinc <br> (D) molybdenum | (C) |
| 603 | 3724 | Which one of the following heads is preferred for high pressure vessels? <br> (A) Torispherical <br> (B) Ellipsoidal <br> (C) Hemispherical <br> (D) Flat plate | (C) |
| 603 | 3725 | Skirt supports are particularly suitable for use with <br> (A) long horizontal vessels <br> (B) small vertical vessels <br> (C) tall vertical vessels <br> (D) short horizontal vessels | (C) |
| 603 | 3726 | The major constituent of natural gas is <br> (A) methane <br> (B) carbon dioxide <br> (C) oxygen <br> (D) nitrogen | (A) |
| 603 | 3727 | The fire of electrical equipments can be extinguished with the use of <br> (A) soda-acid extinguisher <br> (B) carbon dioxide extinguisher <br> (C) foam extinguisher <br> (D) antifreeze extinguisher | (B) |
| 603 | 3728 | Point velocity in a pipeline is measured by <br> (A) Pitot tube <br> (B) Pressure gauge <br> (C) Venturi meter <br> (D) Orifice meter | (A) |
| 603 | 3729 | Laplace Transform of $f(t)=e^{-3 t}$ is <br> (A) $1 /(\mathrm{s}+3)$ | (A) |


|  |  | (B) $1 /(s-3)$ <br> (C) $1 /(s+3)^{2}$ <br> (D) $1 /\left(\mathrm{s}^{2}+3\right)$ |  |
| :---: | :---: | :---: | :---: |
| 603 | 3730 | Write the following set of equations in a matrix form $\begin{gathered} 40=5 x_{3}+2 x_{1} \\ 10-x_{2}=x_{3} \\ 3 x_{2}+8 x_{1}=20 \end{gathered}$ <br> (A) $\left[\begin{array}{ccc} 5 & 2 & 0 \\ 0 & -1 & 1 \\ 3 & 8 & 0 \end{array}\right] \quad\left[\begin{array}{l} x_{1} \\ x_{2} \\ x_{3} \end{array}\right] \quad=\left[\begin{array}{l} 40 \\ 10 \\ 20 \end{array}\right]$ <br> (B) $\left[\begin{array}{lll} 2 & 0 & 5 \\ 0 & 1 & 1 \\ 8 & 3 & 0 \end{array}\right] \quad\left[\begin{array}{l} x_{1} \\ x_{2} \\ x_{3} \end{array}\right] \quad=\left[\begin{array}{c} 40 \\ 10 \\ 20 \end{array}\right]$ <br> (C) $\left[\begin{array}{ll} 5 & 2 \\ 1 & 1 \\ 3 & 8 \end{array}\right]\left[\begin{array}{l} x_{1} \\ x_{2} \\ x_{3} \end{array}\right]=\left[\begin{array}{l} 40 \\ 10 \\ 20 \end{array}\right]$ <br> (D) $\left[\begin{array}{ccc} 40 & 5 & 2 \\ 10 & -1 & 1 \\ 3 & 8 & 20 \end{array}\right] \quad\left[\begin{array}{l} 1 \\ 1 \\ 1 \end{array}\right]=\left[\begin{array}{l} x_{1} \\ x_{2} \\ x_{3} \end{array}\right]$ | (B) |
| 603 | 3731 | The Newton Raphson method for finding the square root of a real number $R$ in the equation $x^{2}-R=0$ <br> (A) $x_{i+1}=\frac{x_{i}}{2}$ <br> (B) $x_{i+1}=\frac{3 x_{i}}{2}$ <br> (C) $x_{i+1}=\frac{1}{2}\left(x_{i}+\frac{R}{x_{i}}\right)$ | (C) |


|  |  | (D) $x_{i+1}=\frac{1}{2}\left(3 x_{i}-\frac{R}{x_{i}}\right)$ |  |
| :---: | :---: | :---: | :---: |
| 603 | 3732 | To solve the ordinary differential equation $3\left(\frac{d y}{d x}\right)+x y^{2}=\sin x, \quad y(0)=5$ <br> by Runge Kutta $4^{\text {th }}$ order method, you need to rewrite the equation as <br> (A) $\left(\frac{d y}{d x}\right)=\sin x-x y^{2}, y(0)=5$ <br> (B) $\left(\frac{d y}{d x}\right)=\frac{1}{3}\left(\sin x-x y^{2}\right), \quad y(0)=5$ <br> (C) $\left(\frac{d y}{d x}\right)=\frac{1}{3}\left(-\cos x-\frac{x y^{3}}{3}\right), y(0)=5$ <br> (D) $\left(\frac{d y}{d x}\right)=\frac{1}{3} \sin x, \quad y(0)=5$ | (B) |
| 603 | 3733 | A partial differential equation has <br> (A) one independent variable <br> (B) two or more independent variables <br> (C) more than one dependent variable <br> (D) equal number of dependent and independent variables | (B) |
| 603 | 3734 | The partial differential equation $5 \frac{\partial^{2} z}{\partial x^{2}}+6 \frac{\partial^{2} z}{\partial y^{2}}=x y$ <br> is classified as <br> (A) elliptic <br> (B) parabolic <br> (C) hyperbolic <br> (D) None of the above | (A) |
| 603 | 3735 | Urea is produced from <br> (A) Ammonia and $\mathrm{CO}_{2}$ <br> (B) $\mathrm{N}_{2}$ and $\mathrm{CO}_{2}$ <br> (C) Methane and CO <br> (D) Natural gas | (A) |
| 603 | 3736 | In Kraft pulping, fibrous material is cooked in the solution of <br> (A) Sodium hydroxide and sodium carbonate <br> (B) Sodium hydroxide and sodium sulphate | (B) |


|  |  | (C) Sodium carbonate and sodium sulphate <br> (D) None of the above |  |
| :---: | :---: | :---: | :---: |
| 603 | 3737 | The equilibrium conversion of SO 2 to SO 3 in a reversible reaction can be increased by $\qquad$ <br> (A) If some amount of SO 3 is removed during intermediate stage <br> (B) If some amount of SO 3 is added during intermediate stage <br> (C) By putting more amount of catalyst <br> (D) None of the above | (A) |
| 603 | 3738 | Ammonia synthesis gas is produced from natural gas by <br> (A) Partial oxidation <br> (B) thermal cracking <br> (C) hydrogenation <br> (D) steam reforming | (D) |
| 603 | 3739 | 10\% Oleum means <br> (A) $10 \mathrm{~kg} \mathrm{SO}_{3}$ and $90 \mathrm{~kg} \mathrm{H}_{2} \mathrm{SO}_{4}$ <br> (B) $10 \mathrm{~kg} \mathrm{H}_{2} \mathrm{SO}_{4}$ and $90 \mathrm{~kg} \mathrm{SO}_{3}$ <br> (C) $10 \mathrm{~kg} \mathrm{SO}_{3}$ and $90 \mathrm{~kg} \mathrm{H}_{2} \mathrm{SO}_{4}$ <br> (D) $10 \mathrm{~kg} \mathrm{H}_{2} \mathrm{SO}_{4}$ and $90 \mathrm{~kg} \mathrm{SO}_{2}$ | (A) |
| 603 | 3740 | The raw materials required in the manufacture of soda ash by Solvay Process are <br> (A) Common salt, lime stone and coke <br> (B) Glauber"s salt,lime stone and coke <br> (C) Common salt,sulphuric acid and lime stone <br> (D) Glauber"s salt, nitric acid and lime stone | (A) |
| 603 | 3741 | Nylon 6 is manufactured from <br> (A) Caprolactum <br> (B) w- amino undeconic acid <br> (C) hexamethylene diamine and adipic acid <br> (D) Phenol | (A) |
| 603 | 3742 | A dissolved solute is to be removed from a solution by stripping with a gas in a packed tower . The height of the packing (Raschig rings) is estimated to be h under a given set of temperature conditions. Which of the following changes in the operating conditions may be done in order to reduce the packing height without reducing the degree of separation.(i) Increasing the operating pressure (ii) decrease the operating temperature and rate of flow of stripping gas (iii) increase the temperature and decrease the pressure (iv) Use saddle packing rather than rings (v) increase the stripping gas rate (vi) add a suitable reagent to solvent that reacts with the dissolved solute <br> (A) (i), (ii) (vi) <br> (B) (ii) <br> (C) (iii), (iv),(v) <br> (D) (vi) | (C) |
| 603 | 3743 | Which of the following packings offer lowest pressure drop? <br> (A) Plastic Raschig ring <br> (B) Metal Pall ring <br> (C) Ceramic intalox saddle <br> (D) Plastic intalox saddle | (B) |


| 603 | 3744 | An orifice type liquid distributer in a packed bed has been installed. But it is tilted. Which of the following problems may occur as a result? <br> (A) Blockage of gas flow through the bed <br> (B) Flooding <br> (C) channelling of liquid <br> (D) All of the above | (C) |
| :---: | :---: | :---: | :---: |
| 603 | 3745 | For a given fluid as the pipe diameter increases, the pumping cost <br> (A) increases <br> (B) remains same <br> (C) may increase or decrease depending upon whether the fluid is Newtonian or non- Newtonian <br> (D) decreases | (D) |
| 603 | 3746 | In which of the electric power generation systems, the operating cost is the minimum? <br> (A) Hydroelectric <br> (B) Thermal <br> (C) Nuclear <br> (D) Fast breeder reactor | (A) |
| 603 | 3747 | Which one of the following is a wrong statement with respect to the distillation column? <br> (A) Operating cost increases if reflux ratio increases <br> (B) Large reflux ratio demands higher heat duty <br> (C) As the reflux ratio increases, the number plates required decreases <br> (D) As the reflux ratio increases condenser cooling load decreases | (D) |
| 603 | 3748 | The quantity of $\mathrm{CO}_{2}$ in atmosphere is increased by <br> (A) vegetation <br> (B) green house effect <br> (C) high winds <br> (D) forests | (B) |
| 603 | 3749 | BOD and COD are the parameters used to assess the quality of <br> (A) Waste water <br> (B) drinking water <br> (C) fertilizer <br> (D) pesticides | (A) |
| 603 | 3750 | Activated sludge process utilizes $\qquad$ for the treatment of wastewater <br> (A) Activated carbon <br> (B) sodium sulphite <br> (C) Fenton reagent <br> (D) microorganisms | (D) |

